

The background of the slide is a close-up photograph of a micro and nanofabrication process. It shows several circular wafers, some with a purple surface and others with a blue surface, arranged in a row. In the foreground, there are several small, clear, cylindrical structures, possibly microfluidic devices or nanofabricated components, resting on a dark surface. The overall scene is brightly lit, highlighting the intricate details of the fabrication process.

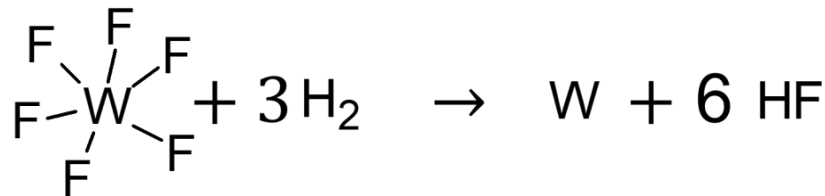
CVD Classroom slides 30 Oct 2024

Micro and Nanofabrication

Prof. hon. Martin A. M. Gijs

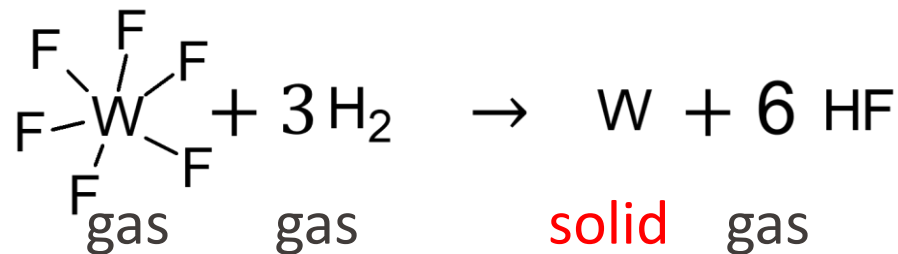
Chemical Vapour Deposition or CVD

- Chemical reaction is involved
- Example for deposition of W at high temperature (600 °C)



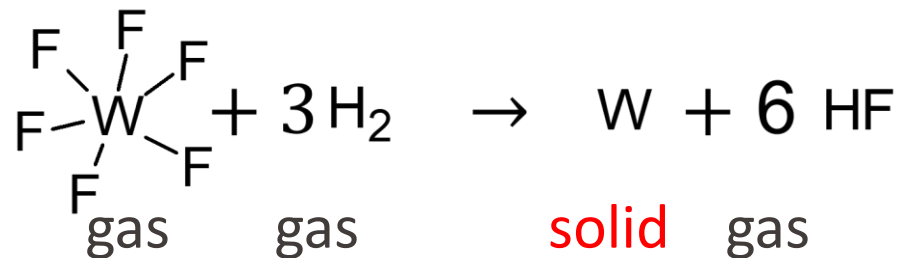
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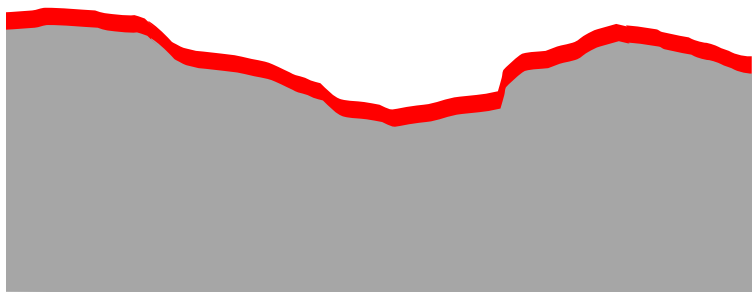


Chemical Vapour **Deposition** or CVD

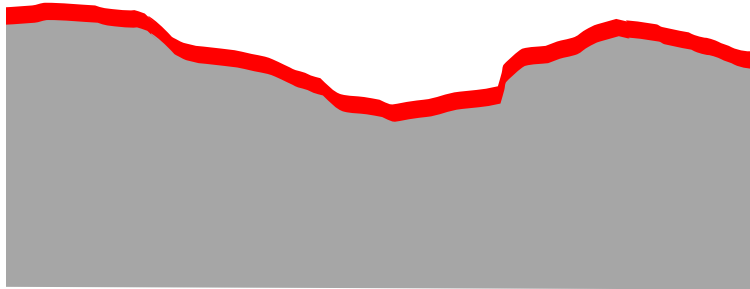
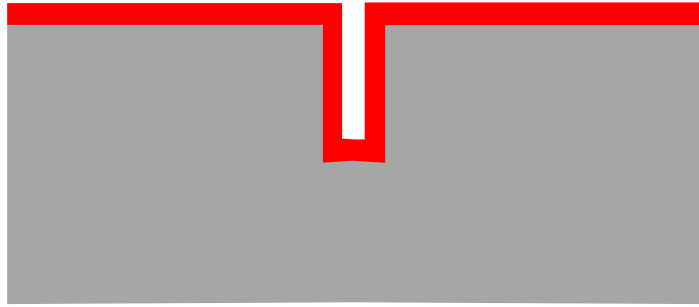
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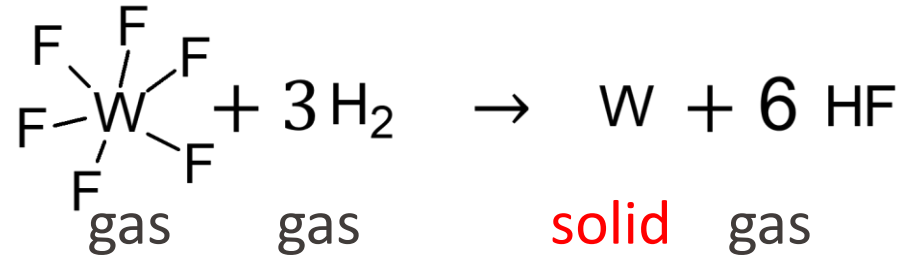
- Use of gaseous phase results in **conformal deposition** on substrate with arbitrary texture



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A Method for Wafer-Scale Encapsulation of Large Lateral Deflection MEMS Devices

Andrew B. Graham, Matthew W. Messana, *Member, IEEE, Member, ASME*, Peter G. Hartwell, J. Provine, Shingo Yoneoka, Renata Melamud, Bongsang Kim, *Member, IEEE*, Roger T. Howe, *Fellow, IEEE*, and Thomas W. Kenny

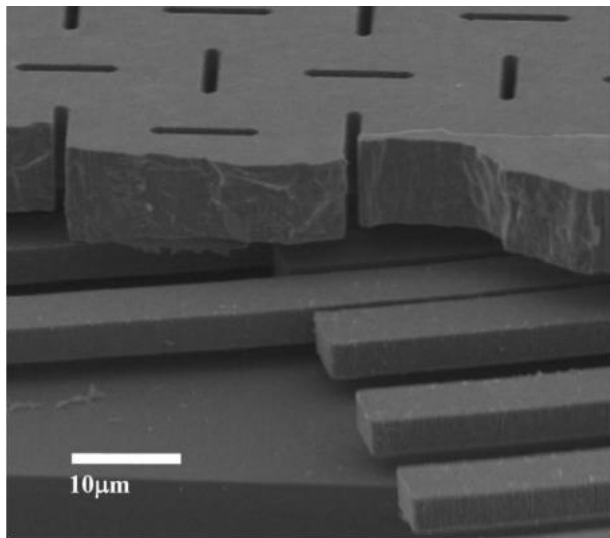


Fig. 11. SEM cross section showing released but unsealed interdigitated comb-drive fingers.

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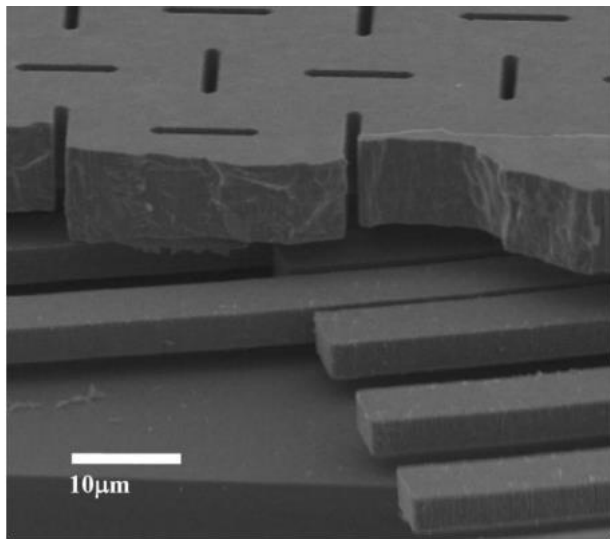


Fig. 11. SEM cross section showing released but unsealed interdigitated comb-drive fingers.

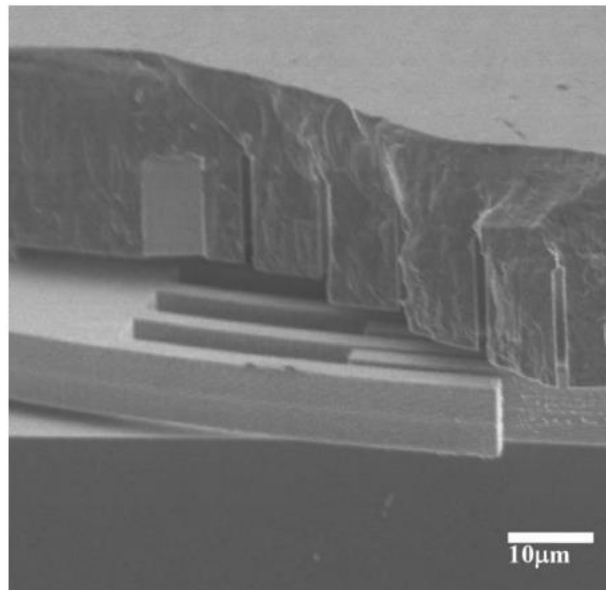


Fig. 12. SEM cross section showing encapsulated and sealed interdigitated comb-drive fingers.

Deposition of SiO_2 by CVD

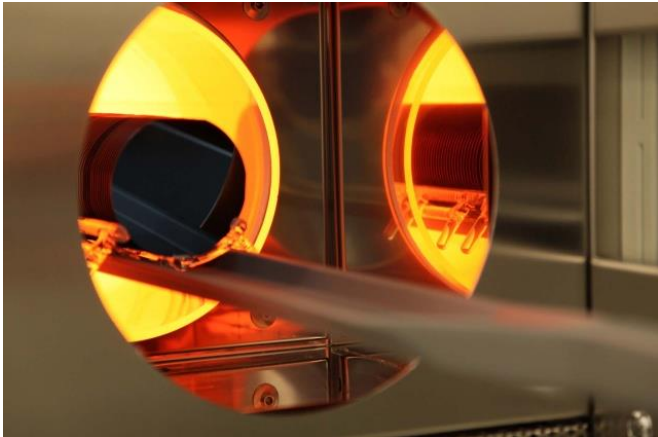
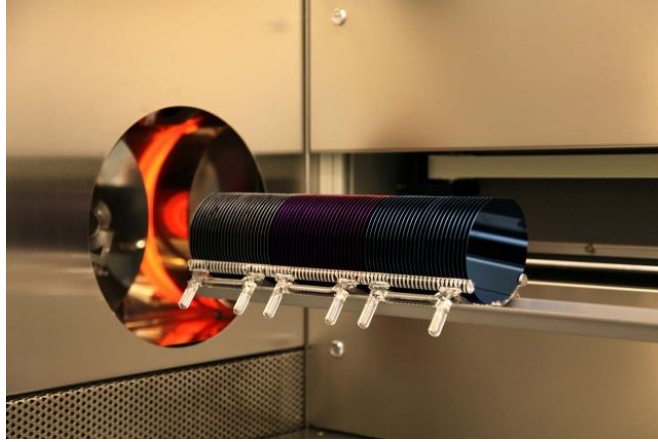
CVD equipment



Example of a thermal CVD reactor



CVD equipment



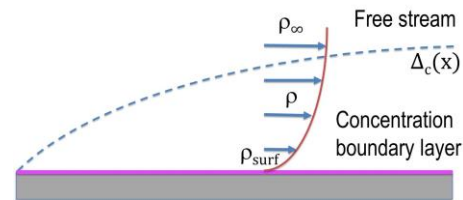
- A batch of Si wafers is positioned in a fused silica holder
- After closing of entrance port, the carrier gas enters the deposition chamber under very controlled flow and temperature conditions
- The CVD thin film is grown on all exposed surfaces of the wafers

Mass transfer from gas phase to substrate

- At equilibrium, the concentration at the surface ($y=0$) is maintained at a uniform value $\rho_{surf} < \rho_{y=\infty}$ and the gas transfer rate per unit surface can be written in three dimensions as

$$\dot{N}[m^{-2}s^{-1}] = h[m\ s^{-1}] (\rho_{surf} - \rho_{y=\infty})[m^{-3}]$$

with h the mass transfer coefficient

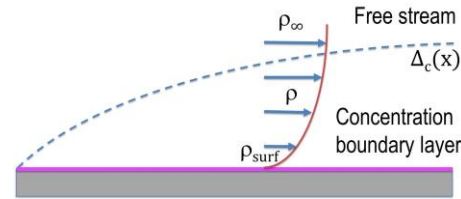


Mass transfer from gas phase to substrate

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- If mass flux associated with species transfer is by **diffusion**, **Fick's law** applies at the surface

$$\dot{N} = -D \left. \frac{\partial \rho}{\partial y} \right|_{y=0}$$

$$h = \frac{-D \left. \frac{\partial \rho}{\partial y} \right|_{y=0}}{(\rho_{surf} - \rho_{y=\infty})}$$

Calculation of the film growth rate

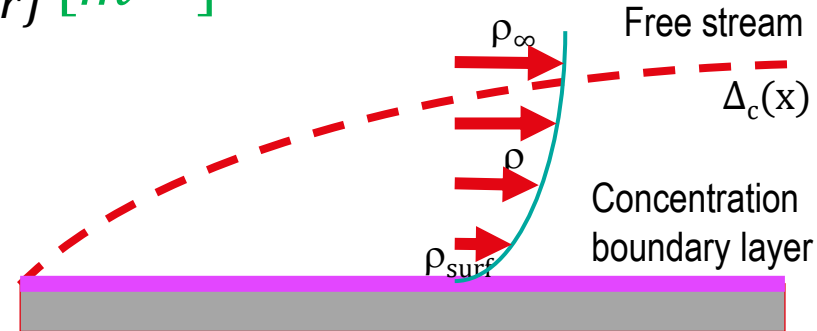
- Diffusion flux of molecules through the boundary layer

$$\dot{N}_1 [m^{-2} s^{-1}] = h [m s^{-1}] (\rho_{surf} - \rho_{y=\infty}) [m^{-3}]$$

- Flux of reacted molecules consumed by the surface reaction

$$\dot{N}_2 [m^{-2} s^{-1}] = -k_{surf} [m s^{-1}] \rho_{surf} [m^{-3}]$$

with k_{surf} the surface reaction rate



Calculation of the film growth rate

- Diffusion flux of molecules through the boundary layer

$$\dot{N}_1 [m^{-2}s^{-1}] = h [m s^{-1}] (\rho_{surf} - \rho_{y=\infty}) [m^{-3}]$$

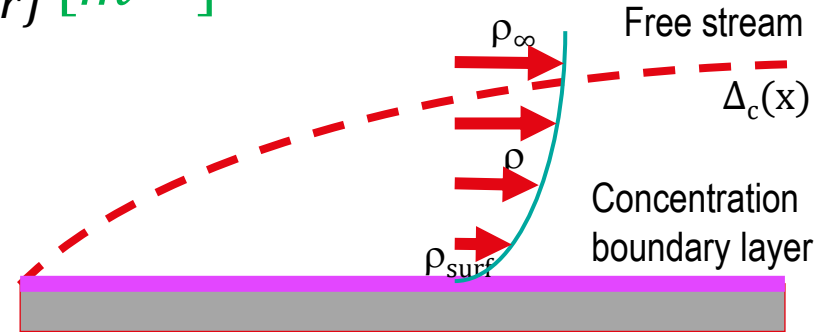
- Flux of reacted molecules consumed by the surface reaction

$$\dot{N}_2 [m^{-2}s^{-1}] = -k_{surf} [m s^{-1}] \rho_{surf} [m^{-3}]$$

with k_{surf} the surface reaction rate

- In equilibrium, $\dot{N} \equiv \dot{N}_1 = \dot{N}_2$, giving

$$\rho_{surf} = \rho_{y=\infty} \left(\frac{h + k_{surf}}{h} \right)^{-1}$$



- The film growth rate is then proportional to

$$\dot{N} = \frac{k_{surf}h}{h+k_{surf}} \rho_{y=\infty}$$

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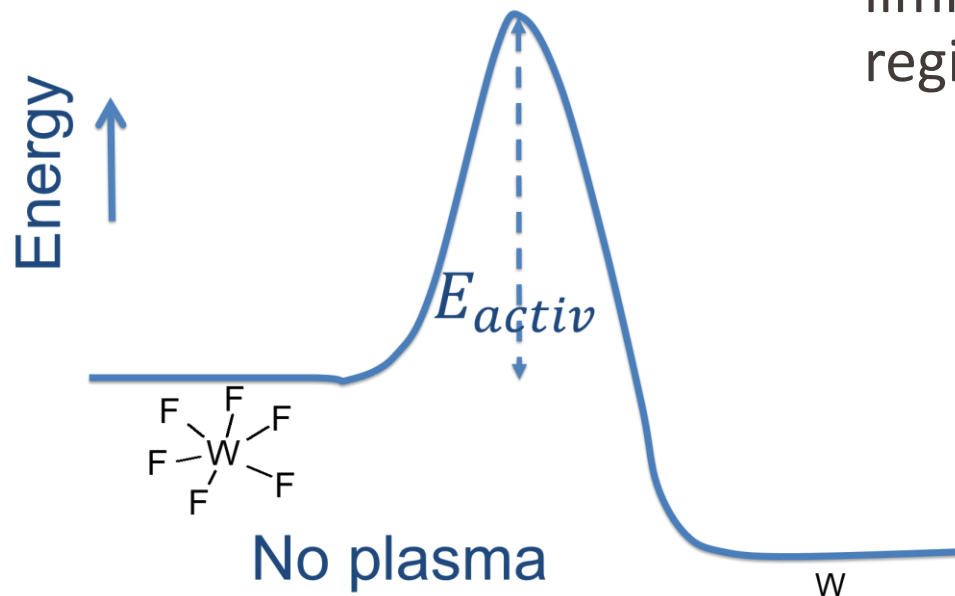
- If $h \gg k_{surf}$, we have the surface reaction-controlled case and

$$\dot{N} = k_{surf} \rho_{y=\infty}$$

- If $h \ll k_{surf}$, we have the diffusion-controlled case and

$$\dot{N} = h \rho_{y=\infty}$$

$$k_{surf} \sim e^{-\frac{E_{activ}}{k_B T}}$$



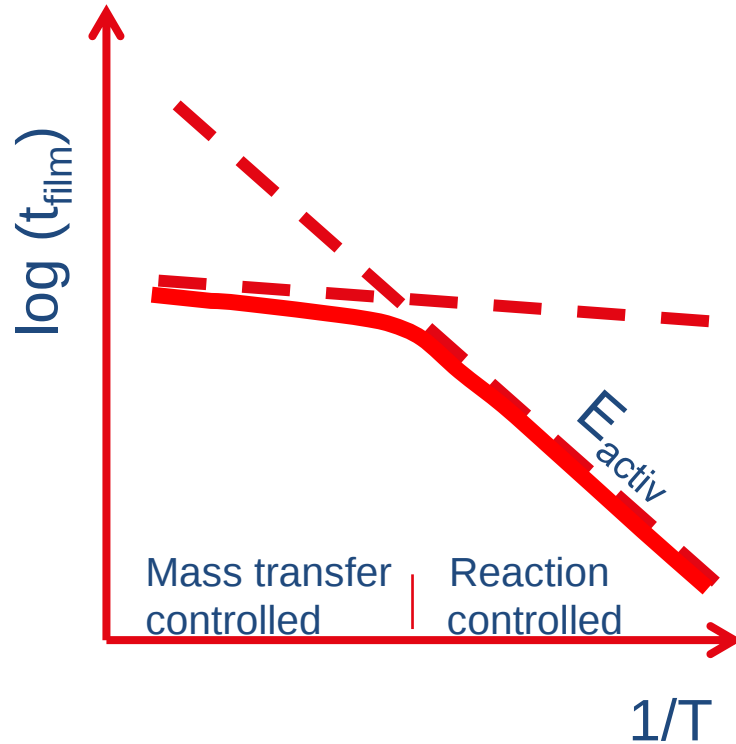
Temperature decides whether film growth is in the reaction-limited or gas diffusion-limited regime

$$t_{film}(x) = C_{gas}(x) \times P_{growth} \times e^{-\frac{E_{activ}}{k_B T}}$$

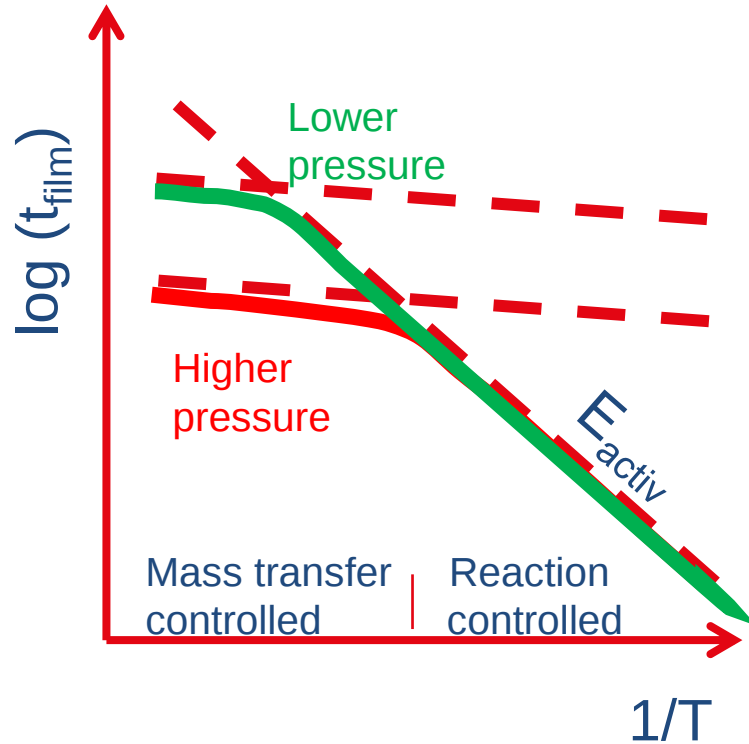
$$k_{surf} \sim e^{-\frac{E_{activ}}{k_B T}}$$

- At high temperature, growth is in the **mass transport-limited regime** → control of gas flow and pressure is crucial for obtaining uniform films
- At low temperature, growth is in the **reaction-limited regime** → control of local temperature is crucial for obtaining uniform films
- A low gas pressure is beneficial for good film uniformity and step coverage

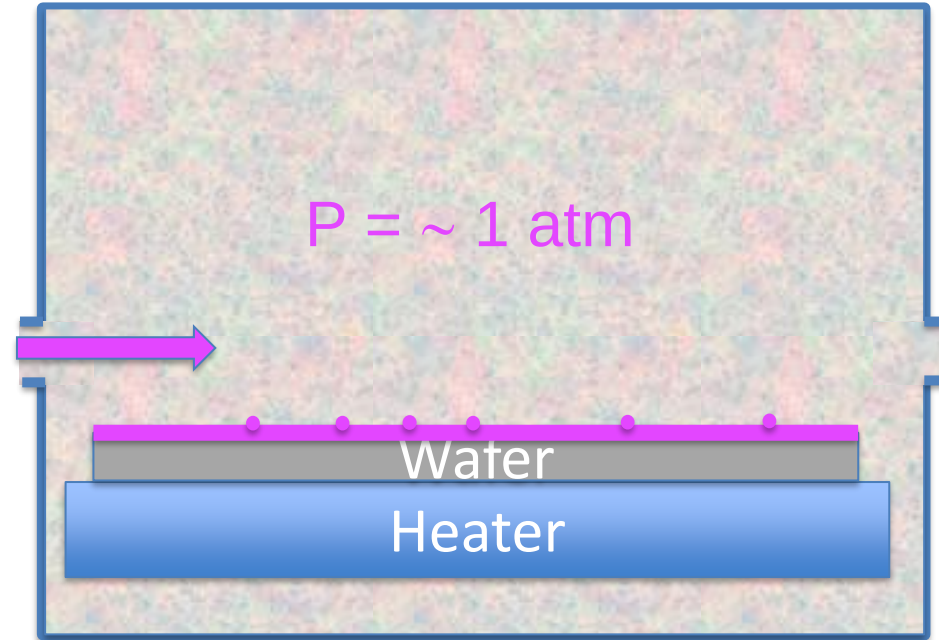
Arrhenius plot of the film growth rate



Arrhenius plot of the film growth rate

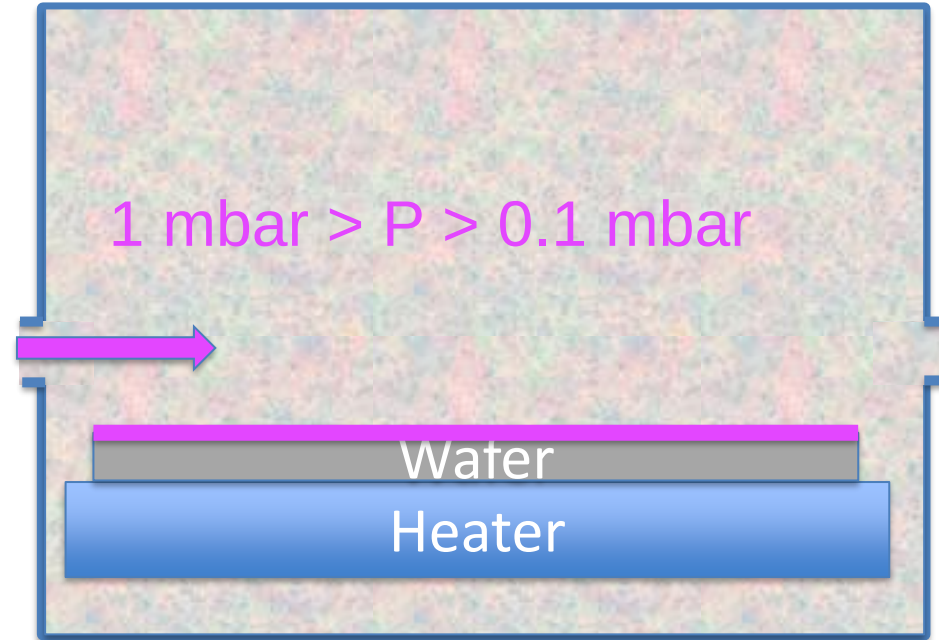


Atmospheric pressure CVD (APCVD)



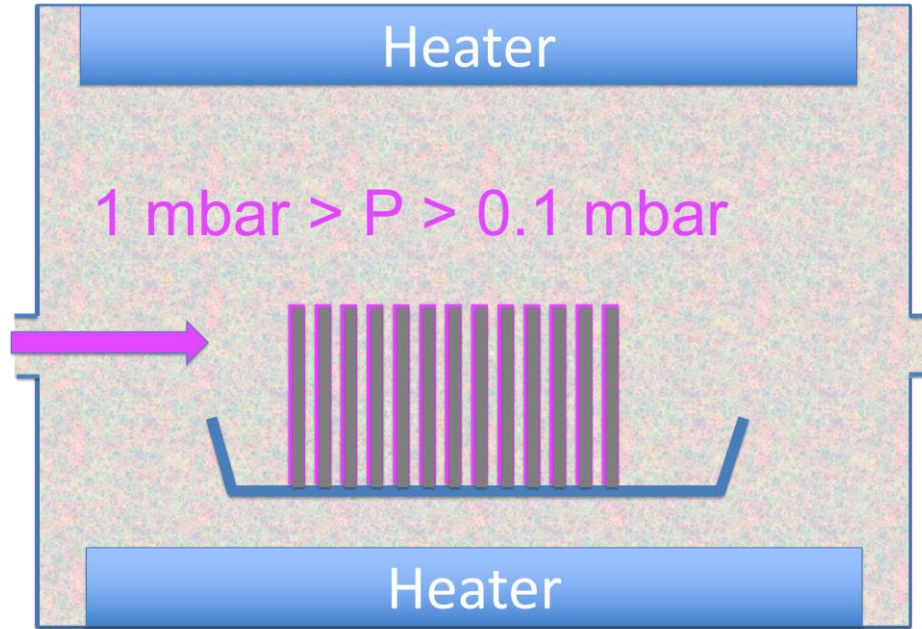
- At high temperature, growth is in the mass transport-limited regime $\rightarrow$ gas flow control is very important
- Wafer placed horizontally in the gas flow $\rightarrow$ limits throughput
- Reaction may already start in the gas phase, resulting in unwanted precipitates on the wafer $\rightarrow$ non-uniformities or pinholes in deposited film

Low-pressure CVD (LPCVD)



- Low pressure results in increased gas diffusion
- No gas concentration gradient perpendicular to flow direction
- More uniform films
- $400\text{ }^{\circ}\text{C} < T < 900\text{ }^{\circ}\text{C}$
- Growth in reaction-limited regime
- Precise temperature control is important
- Usually $10\text{-}100\times$ lower deposition rates compared to APCVD

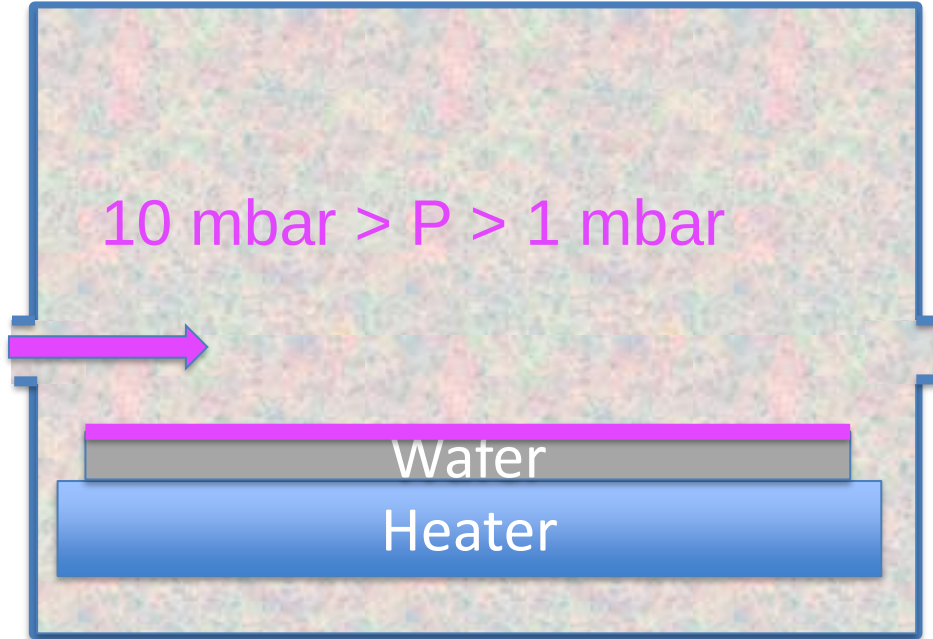
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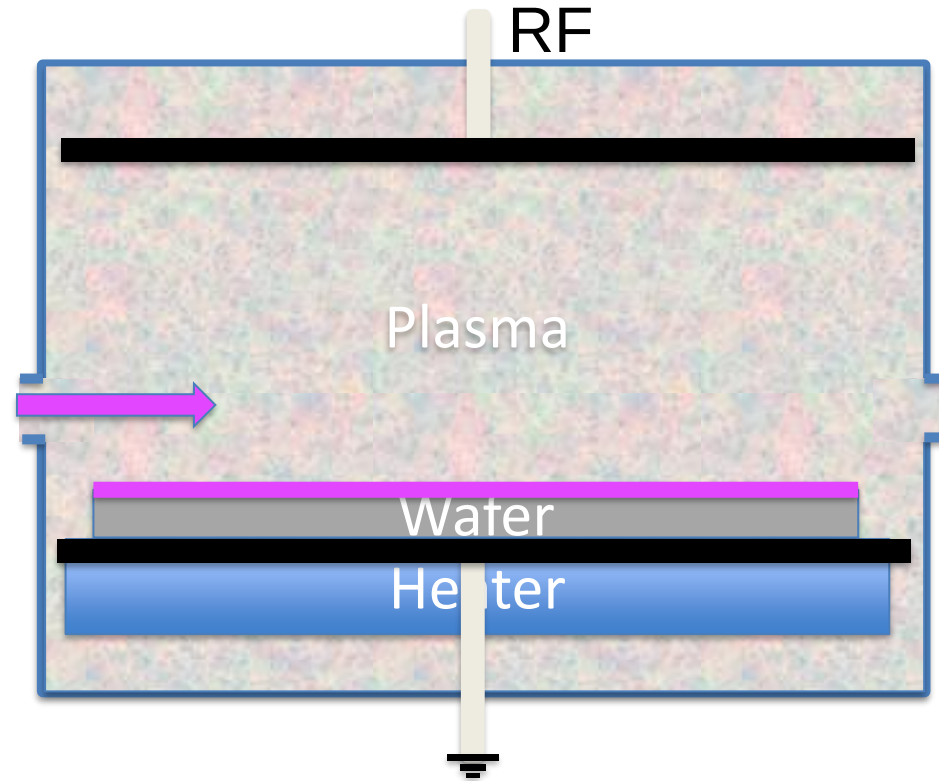
- Wafers can be stacked vertically in batches due to homogeneous gas conditions → wafer throughput can be enhanced
- Downstream depletion of gases can be compensated by establishing a temperature gradient in the heater system

Plasma-enhanced CVD (PECVD)

- Based on LPCVD-like configuration



Plasma-enhanced CVD (PECVD)



- Based on LPCVD-like configuration
- Radio Frequency (RF) power coupled into the gas, typically at 400 kHz or 13.56 MHz
- RF power induces plasma, i.e. a partially ionized gas, containing ions, electrons and excited gas molecules